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Zero Emissions Sulphur Recovery Production

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Zero Emissions Sulphur Recovery Production

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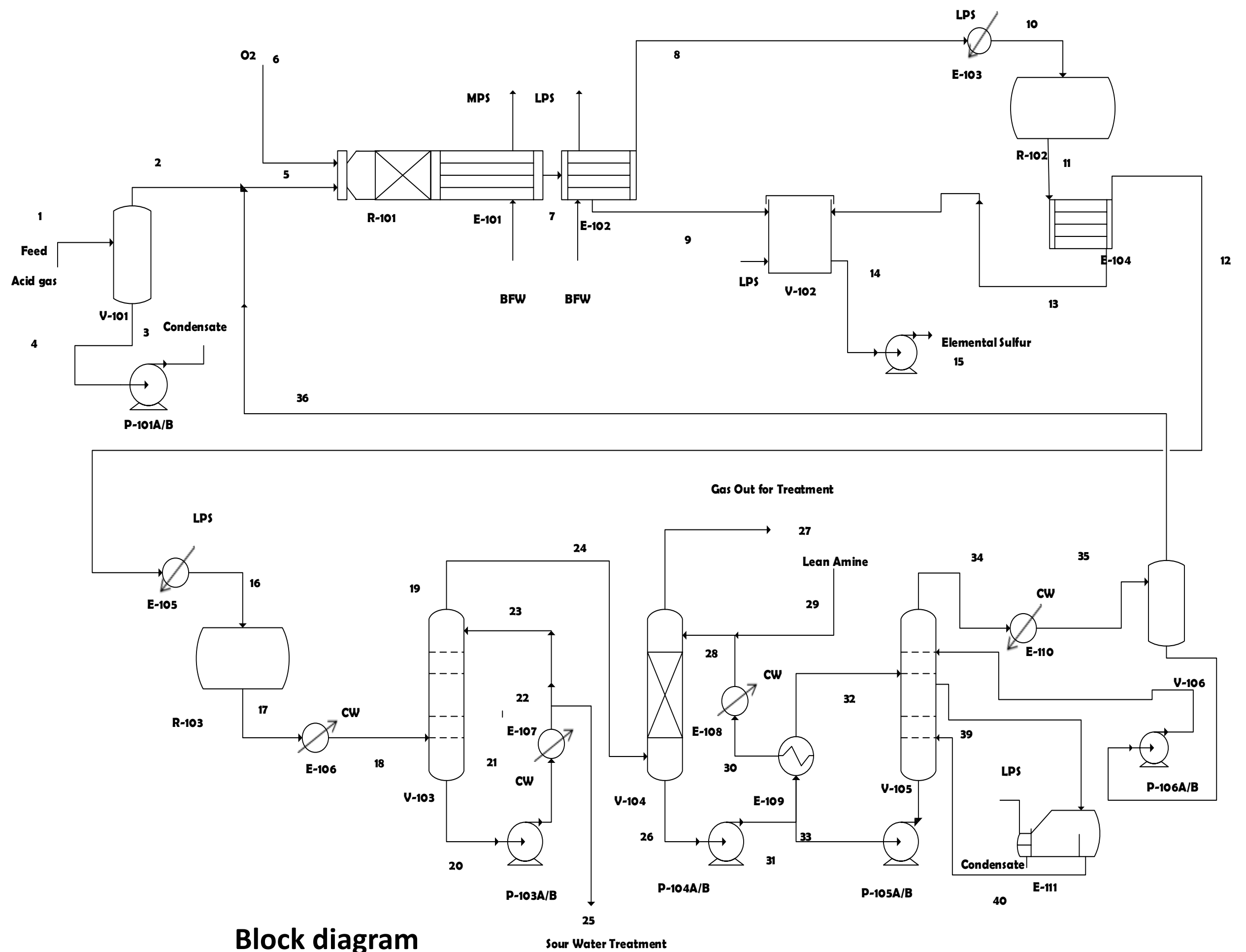
Abstract

A designed process for the concurrent production of hydrogen and Sulphur from a H₂S containing gas stream (acid gas) with zero emissions. The method uses catalytic oxidative cracking, COC, of H₂S to form H₂ and S₂. In addition, the process will have a Claus reactor to reduce the recycle rate of the H₂S to the COC reactor, and a Tail Gas Treatment, TGT, section to produce a rich stream of H₂. As a result, the novelty in the plant is to export H₂ without the necessity of an incinerator.

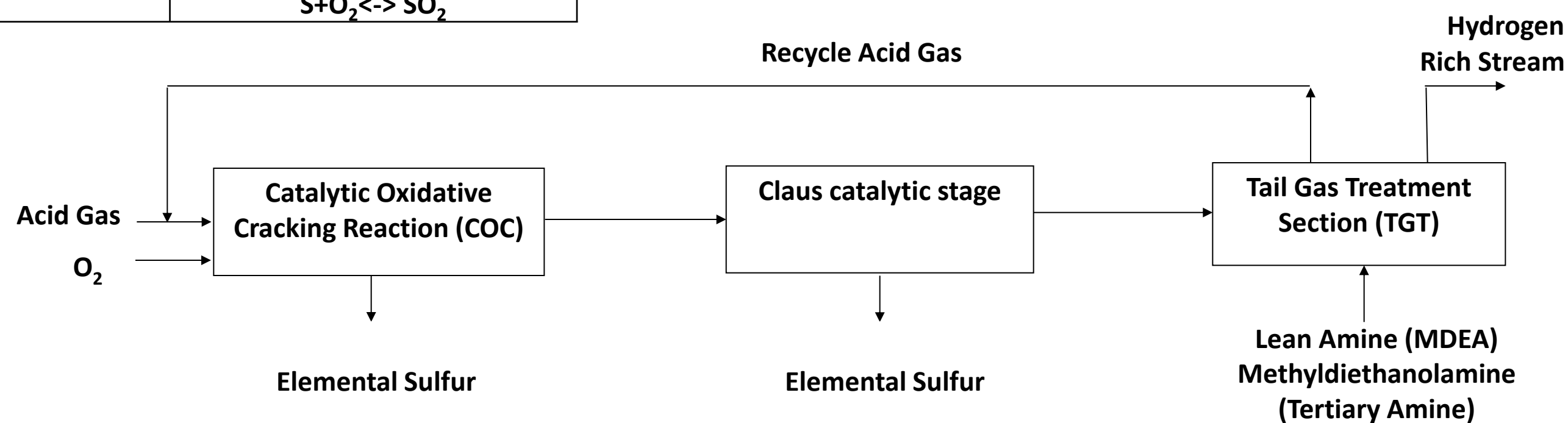
Reactions

Unit	Reaction
Catalytic Oxidative Cracking Reactor (COC)	$4 \text{ H}_2\text{S} + \text{O}_2 \leftrightarrow 2 \text{ H}_2 + 2 \text{ H}_2\text{O} + 2 \text{ S}_2$
	$\text{H}_2\text{S} + 1.5 \text{ O}_2 \leftrightarrow \text{H}_2\text{O} + \text{SO}_2$
	$\text{CH}_4 + 2 \text{ O}_2 \leftrightarrow \text{CO}_2 + 2 \text{ H}_2\text{O}$
	$\text{C}_2\text{H}_6 + 3.5 \text{ O}_2 \leftrightarrow 2 \text{ CO}_2 + 3 \text{ H}_2\text{O}$
	$\text{C}_3\text{H}_8 + 5 \text{ O}_2 \leftrightarrow 3 \text{ CO}_2 + 4 \text{ H}_2\text{O}$
Claus Catalytic Reactor	$\text{H}_2\text{S} \leftrightarrow \text{H}_2 + 0.5 \text{ S}_2$
	$\text{CH}_4 + 2 \text{ S}_2 \leftrightarrow \text{CS}_2 + 2 \text{ H}_2\text{S}$
Hydrogenation reactor	$2 \text{ H}_2\text{S} + \text{SO}_2 \leftrightarrow 1.5 \text{ S}_2 + 2 \text{ H}_2\text{O}$
	$\text{COS} + \text{H}_2\text{O} \leftrightarrow \text{H}_2\text{S} + \text{CO}_2$
	$\text{CS}_2 + 2 \text{ H}_2\text{O} \leftrightarrow 2 \text{ H}_2\text{S} + \text{CO}_2$
	$\text{SO}_2 + 3 \text{ H}_2 \leftrightarrow \text{H}_2\text{S} + 2 \text{ H}_2\text{O}$
	$\text{S} + \text{O}_2 \leftrightarrow \text{SO}_2$

Process Flow Diagram



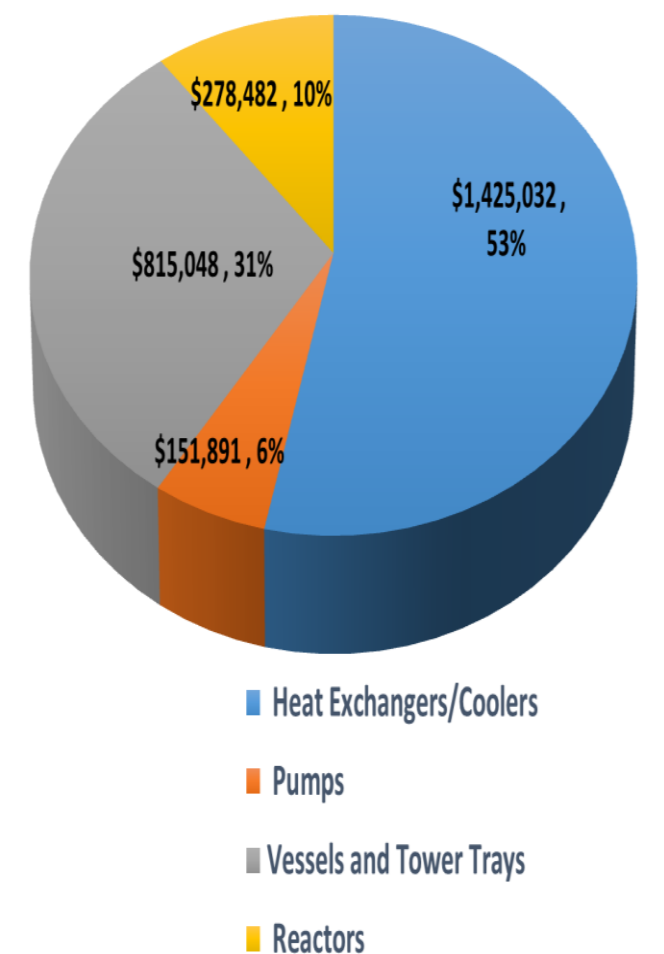
Block diagram



Design Goals

- Elemental Sulphur production rate of 510 ton/day from acid gas feed of 750 kmol/hr and H₂S gas recycle to COC reactor of 512 kmol/hr.
- 309 kmol/hr H₂ rich gas stream of 0.79 mole fraction to be exported to end users.

Equipment Cost Summary



Equipment Used in The Project

Tag Number	Description	Tag Number	Description
V-101	Feed Acid Gas	R-103	Hydrogenation Reactor
V-102	Sulfur Tank	E-101	Waste Heat Boiler
V-103	Quench Tower	E-101	Waste Heat Boiler
V-104	H ₂ S Absorber	E-102	Sulfur Condenser
V-105	Amine Regenerator	E-103	Acid Gas Preheater
V-106	Acid gas Recycle from Amine Regenerator	E-104	Sulfur Condenser
P-101A/B	Condensate Pump	E-105	Gas Pre heater
P-102A/B	Sulfur Pump	E-106	Gas Cooler
P-103A/B	Quench water pump	E-107	Quench Water Cooler
P-104A/B	Rich Amine Pump	E-108	Lean Amine Cooler
P-105A/B	Lean Amine Pump	E-109	Lean and Rich Amine Heat Exchanger
P-106A/B	Acid Gas Recycle Pump	E-110	Gas Cooler
R-101	Air/Oxygen (COC) Reactor	E-111	Amine Reboiler
R-102	Claus Reactor		

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